

Off-Gas Emissions From Vitrification of

Nuclear Waste

Alex Stone, Sheffield Hallam University Transcend Theme Meeting 2020

02/12/2020 Transcend Theme Meeting 2020





The Problem

- The UK has 133,000 m³ of radioactive waste in storage and an estimated 4,420,000 m³ arising in the future¹
- A majority of this waste is from (or will arise from) site decommissioning and legacy (eg. Sellafield, Magnox)
- Vitrification has been considered as a waste treatment technique for ILW which involves the heating of waste to high temperatures up to 1400°C which may volatilise some of the components of the waste²



^{1.} NDA. (2020). *The 2019 Inventory*. NDA Department for Business, Energy and Industrial Strategy. <u>https://ukinventory.nda.gov.uk/the-2019-inventory/2019-uk-data/</u>

^{2.} Caurant, D. (2009). Glasses, glass-ceramics and ceramics for immobilization of highly radioactive nuclear wastes. Nova Science Publishers, Inc.



The Project





Experimental Procedure

- To establish a baseline for validation of the real time system and emission reduction firstly another method must be used to quantify the target gaseous compound
- Impingement³ in various absorption solutions from furnace exhaust and subsequent analysis





Experimental Procedure

Magnesium





Borosilicate



Aluminosilicate

Mixture Windscale



Waste Loading is indicated in the top left of the image.

Clinoptilolite/Sand Mixture







4. Cassingham, N. J., Corkhill, C. L., Stennett, M. C., Hand, R. J., & Hyatt, N. C. (2016). Alteration layer formation of Ca- and Zn-oxide bearing alkali borosilicate glasses for immobilisation of UK high level waste: A vapour hydration study. Journal of Nuclear Materials, 479, 639–646. https://doi.org/10.1016/j.jnucmat.2016.06.009







Conclusion and Future Work

- Off Gas system almost ready for trial runs
- Initial waste glass trials complete with:
 - Simulant contaminated SIXEP sand/clinoptilolite
 - SIXEP sludge
- Good waste loading shown in a number of samples
- Real time system selection and installation into off-gas system
- Collaboration with real time system developers







Simulation of behavioural modification effects in suspension waste pipe flow

Bisrat Wolde, University of Leeds

TRANSCEND Virtual Conference Meeting

2nd December 2020 Virtual Conference





A brief overview of my project:

- Modelling and simulating for Understanding Pond and Silo Sludge Behaviour
- In the decontamination of legacy ponds and silos, the provision of a predictive capability to understand how sludges will behave is crucial to successful retrieval and completion of post operational clean out (POCO) operations
- Develop and validate multiphase direct numerical simulation in a horizontal pipe of radius R, axial length 25R in turbulent flows at Re_{τ} = 361 and 180
- Both polydispersed and irregular shaped particles will be tracked
- Apply behavioural modification effects to the fluid and solid particle properties to promote the desired outcome
- Supervisors: Professor Michael Fairweather

Dr Lee Mortimer





Governing Equations:

 ∂x_n^*

The Navier Stokes equation can be expressed as follows for constant density: $\nabla . u^* = 0$

$$\frac{\partial u^*}{\partial t^*} + (u^* \cdot \nabla) u^* = -\nabla p^* + \frac{1}{Re_b} \nabla \cdot \tau^* + f_i$$

Here, $u^*(x^*, t^*)$ is the fluid velocity vector, non-dimensionalised using the bulk velocity, u_b , the position vector, x^* and time, t^* non-dimensionalized as $x^* = \frac{x}{D}$ and $t^* = \frac{t}{D/u_b}$ respectively, p^* is the non-dimensionalised pressure term for high-velocity flow, $p^* = \frac{p}{\rho u_b^2}$. The bulk Reynolds number Re_b is already a non-dimensional and defined as $u_b D/v$, where, D is the pipe diameter, v is the kinematic viscosity and u_b is the mean bulk velocity, τ^* is the non-dimensionalized stress tensor, $\tau^* = \nabla u^* + \nabla u^{*T}$ and f_i is arbitrary forcing terms used in multiphase flows

A solution for the unknow p, u, v and w is sought using continuity equation, $\nabla \cdot u = 0$ and boundary conditions

The non-dimensional particle equations of motion is given by:

$$\begin{aligned} u_p &= \frac{\partial t^*}{\partial t^*} \\ \frac{\partial u_p^*}{\partial t^*} &= \frac{3C_D |u_s^*|}{4d_p^* \rho_p^*} u_s^* + g * (1 - \rho_p^*) + \frac{3C_L}{4\rho_p^*} (u_s^* x \, \omega_f^*) + \frac{D^{\prime u_f^*}}{2\rho_p^* D t^*} + \frac{Du_f^*}{\rho_p^* D t^*} \\ \\ Drag & Gravity & Lift & Virtual Mass & Pressure Gradier \end{aligned}$$



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Methods:

To solve the descriptive equations numerically a computational fluid dynamics solver Nek5000 used. This solver is based on spectral element method (SEM) – that is a high order weighted residual technique

Nek5000 is favourable for:

- ✓ High spectral accuracy
- ✓ Very little numerical dispersion and dissipation✓ High parallelisation

The high-level computational algorithm is:

- To integrate the Navier Stokes equations, split
- the controlled volume into small cells (meshing)
- Numerically integrate the Navier-Stokes equations throughout the cells
- Solve numerical equations for u, v, w and p in combination with boundary conditions
- Save the solutions for post processing







(a)



(b)



(c)

Computational mesh and pseudo-colour visualisation of the instantaneous axial velocity:

Panels: (a) is the computational mesh with Gauss–Lobatto– Legendre quadrature points (N = 7) for both simulations at Re_{τ} = 180 and Re_{τ} = 361, (b) instantaneous streamwise velocity normalized by bulk velocity, $U_{\rm b}$, (c) a computational mesh clipped at the centreline and pseudo-colour visualisation of the instantaneous axial velocity in 3D







Fluid flow results:

 $Re_{\tau} = 180$

(a) Validation of mean axial velocity profiles at $Re_{\tau} = 180. \ u_z^*$, stream wise direction, _____ solid lines are present DNS contrasted with, - dashed lines are El Khoury's DNS, + cross markers are Den Toonder experiment at $Re_{\tau} \approx 170$ and \circ open circle markers are Eggels experiment at $Re_{\tau} \approx$ 180. (c) Validation of statistical root mean square velocity fluctuation profiles of DNS at $Re_{\tau} = 180$. The axial z_{rms}^* , radial r_{rms}^* , azimuthal θ_{rms}^* , and Reynolds shear stress $< u_z \ u_r >^*$ as a function of $(1-r)^*$ compared against the following DNS and experimental datasets: solid lines are present DNS result, - - dashed lines are El Khoury's DNS, + cross markers are Den Toonder experiment $Re_{\tau} \approx 170$ and \circ open circle markers are Eggels experiment at at $Re_{\tau} \approx$ 180. (b and d) $-\log$ scales.





Fluid results:

$Re_{\tau} = 361$

(a) The mean axial velocity profiles DNS validation at $Re_{\tau} = 361$. u_{z}^{*} solid lines are present DNS contrasted with, – – dashed lines are El Khoury's DNS, u_z^* o open circle markers are Den Toonder experiment at $Re_{\tau} \approx 315$, + cross markers are Singh's DNS. (b) – log scale.

(c) Inner scaled statistical profiles root mean square of fluctuating velcoties of DNS at $Re_{\tau} = 361$. The axial z_{rms}^* , radial r_{rms}^* , azimuthal θ_{rms}^* , and Reynolds shear stress $\langle u_z | u_r \rangle^*$ as a function of $(1-r)^*$ against the following DNS compared and experimental datasets. Solid lines are present DNS result, – – dashed lines are El Khoury's DNS, O, open circle markers are Den Toonder experiment at $Re_{\tau} \approx$ 315 and + cross markers are Singh DNS at $Re_{\tau} \approx 323$. (d) log scale.

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1.4







To investigate the bulk behaviour of high concentration dispersions, a Lagrangian particle tracker has been developed to model large quantities of dispersed solids

- The particles are injected at random position within the fully developed fluid flow domain
- Assigned the fluid velocity at that location
- Particle collision with the pipe wall considered to be elastic
- A fourth order Runge-Kutta method implemented to solve the particle equation of motion for each particle at every time-step
- Statistical data gathered for analysis after letting a few response times to adjust to the surrounding fluid







Particles simulation configurations:

Parameters	Shear Reynolds number, $Re_{\tau} = 361$		Parameters	Shear Reynolds number, $Re_{\tau}^{1} = 140, Re_{\tau}^{2} = 180,$	
	$St^+ \cong 14$	St^+ $\cong 29$	Farameters	<i>St</i> ⁺ ≅ 33	$St^+ \cong 75$
Particle diameter, d_p^+	0.72	0.72	Particle diameter, $\mathrm{d}_p[\mu m]$	60	90
Particle diameter, d_p^*	$2.0E^{-03}$	$2.0E^{-03}$	Particle diameter, d_p^*	$3.0E^{-0.3}$	$4.5E^{-03}$
Axial length	25R	25R	Axial length	25R	25R
Number of particles, N_p	42.0 <i>E</i> ⁺⁰⁴	21.0 <i>E</i> ⁺⁰⁴	Number of particles, N_p	29.4 <i>E</i> ⁺⁰³	43.6 <i>E</i> ⁺⁰³
Shear stokes number, $St_{ au}$	14.4	28.96	Shear stokes number, $St_{ au}$	33.3	75.06
Bulk stokes number, St _b	1.3	2.6	Bulk stokes number, <i>St_b</i>	4.0 ¹ ; 5.45 ²	9.0 ¹ ; 12.27 ²
Density ratio, $ ho_p^*$	5.0 <u>E</u> ⁺⁰²	1.02 100	Density ratio, $ ho_p^*$	$2.058E^{+03}$	$2.058E^{+03}$
Volume fraction, ϕ	$1.79E^{-04}$	8.96 <i>E</i> ⁻⁰⁵	Volume fraction, ϕ	$4.24E^{-05}$	2.12 ⁻⁰⁴
Particle and fluid timestep, Δt^*	$1.0E^{-0.3}$	$1.0E^{-0.3}$	Particle and fluid timestep, Δt [*]	$1.0E^{-03}$	$1.0E^{-03}$



Particle results: $Re_{\tau} = 180$

LPT validation of inner scaled statistical particle (a) mean velocity profiles of a DNS at $Re_{\tau} = 180$, (b) log scale, (c) statistical particle profiles, root mean square of velocity fluctuations of a DNS at $Re_{\tau} = 180$ for axial z_{rms}^* , radial r_{rms}^* , azimuthal θ_{rms}^* and Reynolds shear stress $< u_z \ u_r >^*$ shown. For $St^+ \cong 33$, — solid lines are current work, and + markers are Vreman at $Re_{\tau} =$ 140 DNS, (d) near wall particle concentration of $St^+ \cong$ 33 and 75 normalised by initial bulk concentration and (e) and (f) are corresponding snapshot of the last timestep

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Particle results: $Re_{\tau} = 180$

Probability density function for the particle Reynolds number in viscous, buffer, log-law and bulk flow regions of the pipe at $St^+ \cong 33$ and 75.

Top left is the radial and right is azimuthal. Lower left is the slip velocity and on the right is axial. Solid line: viscous sublayer; dashed: buffer layer; dotted: log-law region; dot- dashed: bulk flow

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Particle results: $Re_{\tau} = 361$

(a) Inner scaled statistical particle mean velocity profiles of a DNS at $Re_{\tau} = 361$, (b) statistical particle profiles, root mean square of velocity fluctuations of a DNS at $Re_{\tau} = 361$ for axial z_{rms}^{*} , radial r_{rms}^* and Reynolds shear stress $< u_z \ u_r >^*$. — Solid line and – – dashed lines are current work, and o and + markers are Sarma DNS, (c) near wall $St^+ \cong$ concentration of particle 14 and 29 particles, normalised by initial bulk concentration, (d) log scale, and (e) and (f) are corresponding snapshot of the last timestep





Particle results: $Re_{\tau} = 361$

Probability density function for the particle Reynolds number in viscous, buffer, log-law and bulk flow regions of the pipe at $St^+ \cong 14$ and 29

Top left is the radial and right is azimuthal. Lower left is the slip velocity and on the right is the axial. Solid line: viscous sublayer; dashed: buffer layer; dotted: log-law region; dot- dashed: bulk flow.

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Dimensional analysis:

$V_c = f(d, D, \phi, (\rho_s - \rho_f)g, \rho_f, \mu)$

Where, $\mu = [ML^{-1}T^{-1}] - Dynamic viscosity$ $g = [LT^{-2}] Acceleration due to gravity$ $V_c = [LT^{-1}] \text{ critical velocity}$ d = [L] particle diameter D = [L] pipe diameter $Q_s = [L^3T^{-1}] \text{ solid-phase volumetric flow rate}$ $Q_f = [L^3T^{-1}] \text{ solid-phase volumetric flow rate}$ $\rho_s = [ML^{-3}] \text{ Density of solid phase}$ $\rho_f = [ML^{-3}] \text{ Density of fluid phase}$

Side note: $\phi = \frac{Q_s}{Q_s + Q_l} = [M^0 L^0 T^0] = [1]$ and $s = \frac{\rho_s}{\rho_f} [M^0 L^0 T^0] = [1]$

To develop a functional relationship the above equation set to:

$$\frac{V_c}{\sqrt{gd(s-1)}} = i_0 (\frac{d}{D})^{i_1} \phi^{i_2} (1-\phi)^{i_3} (\frac{\mu}{d\rho_f \sqrt{gd(s-1)}})^{i_1}$$

 $i_0 - i_4$ values determined by regression using experimental data.

The following model derived using linear regressor is:

$$\frac{V_c}{\sqrt{gd(s-1)}} = 1.85 \left(\frac{d}{D}\right)^{-0.18} \phi^{0.154} \left(1-\phi\right)^{0.16} \left(\frac{\mu}{d\rho_f \sqrt{gd(s-1)}}\right)^{0.09}$$
(Eq 1

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For a Low Carbon Futur

Experimental deposition data were also plotted against the same empirical correlation (equation 1.) Deposition based dataset plotted against the same empirical correlation.

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Planned work:

- Validation of particle deposition
- Deploy two-way coupling
- Investigate the settling and deposition behaviour of suspensions of dense particles
- Implement four-way coupling
- Implement four-way coupling with agglomeration
- DLVO theory will be applied

- Modelling and understanding pond and silo sludge behaviour
- Apply behavioural modification effects to the fluid and solid particle properties to promote the desired outcome such as reducing particle agglomeration, and hence, the likely deposition of particles during processing
- The behavioural modification effects to be studied includes changes in:
- Temperature
- ✤ Ionic strength
- Polymers and pH of the liquid phase





Any questions?





Thank you

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The University Of Sheffield.



Characterisation of Thermal Treatment Products

Project Overview and First Year Review (January 2020-December 2020)

Daniel Parkes, University of Sheffield (dparkes2@sheffield.ac.uk) TRANSCEND November 2020





Compacted and cemented PCM waste

Project Drivers

- NDA strategy integrated and optimised waste management strategy
- HLW (High Level Waste)—encapsulate in borosilicate glass. No Change.
- ILW (intermediate Level Waste)—fragmented, mostly compaction and cement. Thermal treatment advantages reduction in volume and reactivity. Main Focus.
- LLW (Low Level Waste) –compaction, incineration and metal decontamination. No Change. but interest due to ILW/LLW boundary waste.



October 2015





Plasma Vitrification set up at Valingar, Swindon

ILW and Thermal Treatment

- Thermal technologies plasma vitrification, joule heating (JHCM and Geomelt), induction melting, incineration, SHIVA, PIVIC.
- UK ILW Sand-Clino, Magnox Sludge, Plutonium Contaminated Material (PCM) and mixed alpha and beta waste.

- Graphite
- Plutomium contaminated material
- Conditioned
- Contaminated metals
- Activated metals
- Contaminated other materials
- Others
- Fuel cladding and miscellaneous waste
- Flocs
- Mixed wastes

UK ILW compositional percentage mix



<u>Aims</u>

- **Treatment process** –experiments, processing temperature, waste composition, glass frit composition, processing time- literature review.
- Composition non reactive, durable, homogenous.
- Radionuclide distribution concentration, glass, metal, crystalline material, homogenous.
- Long term durability dissolution, disposal safety case.



<u>Plans</u>

<u>Samples</u>

- Lab simulants build on previous studies (*L.Boast PhD* and *Hyatt 2013*) create lab simulants of previous studies for comparison to industry/archaeological samples. Create new samples with updated glass frit.
- Industrial samples Valingar for Sellafield.
- Archaeological samples Hayle, Cornwall. Copper smelting slag immersed in saline waster for 209 years. Previous analysis shows slag analogous to PCM, investigate long term dissolution behaviour.

<u>Techniques</u>

- Characterisation Sample composition glass and crystalline composition (SEM, XRD, XRF, Mossbauer) radionuclide distribution, partitioning, oxidation state (SEM, XANES, XRF), metal composition – decontamination and oxidation.
- **Dissolution Experiments** standard PCT to look at bulk dissolution but also VCI (Vertical Scanning Interferometry) to look at dissolution of different glass and crystalline elements of the waste form.



Examples - Samples

- COVID issues with lab access
- Other samples WANTED please email dparkes2@sheffield.ac.uk





Examples – Techniques

COVID issues with lab access – examples from L.Boast PhD.

- SEM images show mixed Xc and glass.
- EDX maps potential even radionuclide distribution.
- EDX data 1.2 mol% CeO₂ in amorphous phase – upper limit 2 mol%.





• XRD identifies mineral phases







- PCT dissolution tests with normalised loss for Si
- PVC waste reduced durability due to lower SiO₂ so reduced network connectivity.



Thankyou for listening

And thankyou to:

Dr Claire Corkhill (UoS) Dr Clare Thorpe (UoS) Mike Harrison (NNL)



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Processes at and across Nanoparticle-Water

Interfaces

Ella Schaefer, UoM

Integrated Waste Management Theme

2.12.20 ella.schaefer@postgrad.manchester.ac.uk







Background



Figure 1 – Diagram showing the irradiation of a NP resulting in various radiolytic species, noting two of interest; the hydroxyl radical and gaseous dihydrogen, and their relevance to key fields.



Aims

- Develop simulations where energy is directly deposited into NPs
- Model energy transfer at the NP-water interface
- Cultivate an integrated account of all processes



Background



Figure 2 – The three classes of pathways for irradiated NP solutions [Sicard-Roselli, et al Small. 2014;10(16):3338–46.].



Background



Figure 2 – The three classes of pathways for irradiated NP solutions.


Pathway B – Water Radiolysis



Figure 3 – The three stages of water radiolysis. [Le Caër S, 2011;3(1):235–53.].





Figure 2 – The three classes of pathways for irradiated NP solutions.



Pathway A – Interaction with the NP

NP is irradiated creating a range of energetic species:

- Photoelectric effect
 - Esp. Auger cascade
- Excitons







Figure 4 – Auger emission diagram [A. Carlson, 2007]



Figure 5 – Diagram depicting the formation of an exciton by the excitation of an electron from the valence band to the conduction band.





Figure 2 – The three pathways for irradiated NP solutions.



Pathway C – NP interface

Mechanisms that occur at the NP-water interface which lead to water radiolysis:

- Structured water layers lengthen H-OH bonds
- Energy carrying species interact with surface
- Pathways A and B still occur



Aims

- Develop simulations where energy is directly deposited into NPs
- Model energy transfer at the NP-water interface
- Cultivate an integrated account of all processes





Figure 6 – A visualisation of the simulation procedure for the second model



Preliminary Results



Figure 7 – Graphs showing the radial dose distributions per incident photon for a) Au, b) AI_2O_3 , c) Mg(OH)₂ and d) Water NPs irradiated by 50, 100, 150, 250 and 500 keV photon beams.



Preliminary Results







Figure 8 – Graphs showing the radial dose distributions per incident photon for a) AI_2O_3 , b) Mg(OH)₂ and c) Water NPs irradiated by 10, 15, 20 and 30 keV photon beams.



Future Work

- Investigate which effects are dominant in Al₂O₃ and Mg(OH)₂
 - Photon energy
 - Density
 - Atomic number
 - NP size
- Develop scorer that can detect and track ionisations and excitations
- Model water radiolysis
- Simulate exciton mechanism for energy transfer





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Imperial College London

Nanotechnology for effluent treatment and radionuclide assay

Dr. Gurpreet Singh Imperial College London Supervisors: Prof. Luc Vandeperre & Prof. Mary Ryan

02/12/2020 TRANSCEND Project



Previous Works

Proposed developments

- Fortner's group (ref 1) had reported since 2015 about magnetic nanoparticles of mixed Mn/Fe oxide nanocrystals covered with a bilayered oleyl phosphate to adsorb/exchange uranyl ions in solution.
- Adsorption Capacity reported to be 1667 mg/g of mixed oxide nanocrystals.
- In 2018 Imperial's PhD student (Ref 2) further enhanced the work by using pure magnetite coated with oleic acid (12nm in size).



- The nanoparticles were further functionalised with phosphate groups to sequester uranium.
- The reported uptake capacity of Uranyl ions at neutral pH 7 was 1700 mg/g of Fe in 200ppm U(VI) nitrate solution
- This is the highest ever to be reported in the

The TRANSCEND project is aimed at the following:

- 1. To understand the mechanism of adsorption
- 2. To extend the application at acidic pH
- 3. To target other radionuclides with new functionalised coatings
- 4. To investigate magnetic steering of nanoparticles for repairing cracks in concrete





Work so far

- Previous method has limitations to upscale, especially due to tedious synthesis protocols and time frame. Hence, a new methodology is investigated using co-precipitation and microemulsion processes.
- The new process under investigation is lacking homogeneity, as currently the size of particles is between 5nm to 25nm, with a higher degree of aggregation.
- Current synthesis time is 3 hours from scratch, in regard to the 30+ hours of previous work.
- Current synthesis is easily up-scaled to any volumes required.
- The cost of production is presumed to cheaper, if the protocol is perfected.
- Yet to Validate the protocols and perform further analysis and adsorption experiments.





Top Image: Previous work of oleic acid coated (left) & phosphate-coated magnetite (right)



Bottom Image: Current work of bare-magnetite



REFERENCES

 Wenlu Li, John T. Mayo, Denise N. Benoit, Lyndsay D. Troyer, Zuzanna A. Lewicka, Brandon J. La⊄erty, Je⊄rey G. Catalano, Seung Soo Lee, Vicki L. Colvin, and John D. Fortner. Engineered superparamagnetic iron oxide nanoparticles for ultra-enhanced uranium separation and sensing. J. Mater. Chem. A, 4(39):15022– 15029, 2016.

2. Calì, E. & Qi, Jiahui & Preedy, O. & Chen, S. & Boldrin, D. & Branford, Will & Vandeperre, L. & Ryan, M. (2018). Functionalised magnetic nanoparticles for uranium adsorption with ultrahigh capacity and selectivity. Journal of Materials Chemistry A. 6. 10.1039/C7TA09240G.





Scoping studies of ion exchange materials

James Reed, University of Birmingham

2.12.2020 Virtual conference





About Me

- Msci Chemistry graduate, University of Birmingham.
- Particular interest in ion-exchange materials and materials chemistry.
- Enjoy running
- Keen cricketer







Msci Project: Magnetisation of tin umbites







Current work: 2nd year PhD student, Hriljac/ Allan group

- 3 ½ years supported by Sellafield Ltd and NNL.
- Aim: to improve ion-exchange characteristics of naturally sourced zeolites by chemical treatments.
- Includes desilication and dealumination of the zeolite framework and phase transformations to improve uptake.



Sellafield Ltd





Why caesium and strontium?

- Cs-137 and Sr-90 are key targets in removal from nuclear waste streams worldwide.
- At the Sellafield site, SIXEP treats 100s m³ per day.
- Currently utilises a clinoptilolite sourced from Mud Hills in California.
- Supply limited, new materials must be sourced.







Zeolites



(Or Al)



- Cations balance this charge by sitting in spaces/ pores within the framework.
- These ions are free to move and can therefore take part in ion-exchange processes.



High Al content: high cation capacity

Used in ion-exchange





Interzeolite Transformations

• Uses a zeolite framework as a starting material to form a different structure



- Changes selectivity
- Increases purity
- Can add value to 'low value' materials



MH-CLINO (HEU)



Cs: 84 % uptake Sr: 46 % uptake

Z-CLINO (HEU)



Cs: 69 % uptake Sr: 27 % uptake

I-MORD (MOR)



Cs: 93 % uptake Sr: 7 % uptake

- Caesium uptake good to excellent in all systems.
- Strontium uptake poor, especially in mordenite.
- Improvement in strontium uptake required.







Chabazite (CHA) Cs: 3 % Sr: 98 %



Monoclinic unit cell a = 17.52 Å, b = 17.04 Å, c = 7.40 ÅFD = 17.5 T/1000 Å³ 10 and 8 ring channels along [001]



Trigonal unit cell a = b = 13.68 Å, c = 14.77 ÅFD = 15.1 T/1000 Å³ 8 ring channels along [100] and [010] 6 ring channels along [001]



Z-CLINO (HEU) Cs: 69 % Sr: 27 %



Zeolite-P (GIS) Cs: 84 %

Sr:61 %



Monoclinic unit cell a = 17.52 Å, b = 17.04 Å, c = 7.40 ÅFD = 17.5 T/1000 Å³ 10 and 8 ring channels along [001]



Tetragonal unit cell a = b = 9.80 Å, c = 10.16 ÅFD = 16.4 T/1000 Å³ 8 ring channels along [100] and [010] TRANSCEND

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- No phase change of starting materials when KOH is used.
- Reason for this divergent phase selectivity investigated through different treatments.



GIS







Orthombic unit cell *a* = 18.26, *b* = 20.53 Å, *c* = 7.54 Å FD = 17.0 T/1000 Å³ 12 and 8 ring channels along [001]



Tetragonal unit cell a = b = 9.80 Å, c = 10.16 ÅFD = 16.4 T/1000 Å³ 8 ring channels along [100] and [010]



Interzeolite phase transformations of three starting materials





Partial transformations



- Would this retain some selectivity from the parent zeolite?
- If so, this could lead to valuable selectivity profiles.
- Concern over physical stability of parent zeolite.















PP bottle transformations









An in-depth look at generating composites

- Series of composites generated by varying [NaOH].
- Weight fractions of each phase obtained through Rietveld refinement of powder diffraction data.

• Potential to 'tune' material for a given waste stream.

For Z-CLINO:





TBAH as an alternative reagent





Future work:

- Ion exchange data on composite studies
- Generate composite series for I-MORD
- Microscopy studies to further characterise materials
- Bring in new materials to examine
- More use of TBAH
- Active testing





[1] A. Dyer, J. Hriljac, N. Evans, I. Stokes, P. Rand, S. Kellet, R. Harjula, T. Moller, Z. Maher, R. Heatlie-Branson, J. Austin, S. Williamson-Owens, M. Higgins-Bos, K. Smith, L. O'Brien, N. Smith and N. Bryan, Journal of Radioanalytical and Nuclear Chemistry, 2018, 318, 2473-2491.

[2] <u>https://theconversation.com/why-cant-we-predict-when-a-volcano-will-erupt-53898</u>

[3] Images taken from Google earth



Thank you

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Improving *in situ* acoustic characterisation of suspensions with machine learning methods

Joe Hartley, University of Leeds

Theme 1 – Integrated Waste Management

02/12/2020 Joint Nuclear Event Webinar







Background

- Graduated from the University of Sheffield in 2019.
 - 2.1 Material Science and Nuclear
 Engineering MEng.
 - FYP: A Dissolution Study of Thermally

Treated Chabazite By Hot Isostatic Pressing.

- October 2020: Started PhD at University of Leeds:
 - Advanced Ultrasonic Characterisation of Slurry Flows



Research Challenge

- ILW legacy sludge at Sellafield needs to be pumped out of ponds to be processed.
- Characterisation data on the sludge is scarce;
 - Remote online monitoring system is needed to characterize the sludge during pipe-

flow.

Figure 13: Composition of ILW by waste group



Graphite 66,000 m³

- Plutonium contaminated material 38,700 m³
- Conditioned 26,600 m³
- Contaminated metals 25,600 m³
- Activated metals 18,400 m³
- Contaminated other materials 17,100 m³
- Others 15,100 m³
- Fuel cladding & miscellaneous wastes 14,600 m³
- Flocs 14,200 m³
- Mixed wastes 11,000 m³





https://ukinventory.nda.gov.uk/wp-content/uploads/2020/01/2019-Waste-Report-Final.pdf https://www.youtube.com/watch?v=Yu7-D37SKOY&ab_channel=SellafieldLtd



Similar Use of Acoustics

Acoustic Backscatter System has been used industrially to characterise slurries:



P.D. Thorne, D.M. Hanes / Continental Shelf Research 22 (2002) 603–632



Thorne, Hanes; A reveiw of acoustic measurement of small-scale sediment processes

DOI:10.1016/j.mineng.2011.12.003

DOI: 10.1016/j.ces.2014.11.063



Acoustic Instrumentation

- UVP-DUO from Met-Flow.
- Has been used in the department for nearly a decade good expertise.
- Frequency range from 1–8 MHz
- Active radii for the transducers are 2.5 10 mm; 2.5 or 5 mm is ideal for non-intrusive attachment on pipelines.





UVP Monitor Model UVP-DUO With Software Version 3, User's Guide, Draft Ed., Met-Flow, Release 5, 1/07/02.



ML and How It Will Be Applied

- Machine Learning:
 - making the computer learn
 from studying data and
 statistics.
 - a step into the direction of artificial intelligence (AI).
 - program that analyses data and learns to predict the outcome.
- Essentially pattern matching
 'test' data to the 'training' data.





https://www.python.org/static/community_logos/python-logo-master-v3-TM.png | https://whimsical.com/machine-learning-roadmap-2020-CA7f3ykvXpnJ9Az32vYXva



Overview of Project Objectives

- Understand current Acoustic Backscatter (AB) performance of UVP for characterisation of nuclear suspension in slurry pipe-flows.
- Investigate Machine Learning (ML) methods to improve UVP particle aggregate size and concentration measurements.
- Investigate the effect of large molecular weight polymers on the AB performance of UVP.
- ➢ Compare/ combine FBRM measurements to/ with UVP-DUO and ML system.
- Understand influence of discrete size fractions, as well as varying discrete size fraction mixes, and how ML is affected.
- Optimise system to give real-time results for real-time flocculation.



Thank you

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Simulation of behavioural modification effects in particle-laden flows Computational modelling of interacting polymer additives



Lee Mortimer, University of Leeds

Prof. Mike Fairweather, University of Leeds

2nd December 2020 Online meeting

TRANSCEND / NDA VIRTUAL CONFERENCE 2020





MOTIVATION

- Waste suspension flows transport legacy material from historic ponds to other interim locations where they are stored safely.
- Present designs perform inefficiently, with the potential for blockages and poor flow conditions.
- Current transportive systems may not function adequately for long timeframes.
- Presence of high flow rates means systems are usually turbulent, leading to complex chaotic behaviour.
- Knowledge must be developed surrounding behaviour of waste sludges.
- Generation of this knowledge will lead to accurate predictive capabilities and enhanced control over multiphase turbulent flows.

Behavioural modification



DEVELOPMENT OF BEHAVIOURAL MODIFICATION TECHNIQUES

- Use high-fidelity simulation to predict system response to modification-capable properties.
- Temperature, ionic strength, pH, material coating, presence of other phases (particles/polymers), flow rates, turbulence intensity.
- Explore fundamental dynamics surrounding interaction mechanisms such as:





MULTIPHASE FLOW SIMULATION TECHNIQUES

Range of technical tools for both the fluid and particle phases

FLUID PHASE

Direct numerical simulation (DNS):

- All relevant turbulent length and timescales are resolved.
- Accuracy and high-fidelity allows for investigation of fundamental dynamics.
- Computationally intensive but code is parallelised (HPC at Leeds).
- NEK5000 open source spectral element method solver.

PARTICLE PHASE

Lagrangian particle tracking (LPT):

POLYMERIC PHASE

Finitely extensible nonlinear elastic (FENE) bead-spring model



POLYMER-LADEN SHEAR AND TURBULENT FLOWS

Computational investigation into the use of polymer additives for beneficial modification of slurry flow behaviour







Polymers – a recap

- Polymers are chemical compounds with molecules bonded together in long repeating chains of monomers.
- Both synthesized and naturally occurring.
- Possess **important advantageous properties** surrounding the way in which they interact with both themselves and other materials.
- In the present case, we are interested in how they **interact** and beneficially **modify behaviour** of both the fluid and particles.



Super-resolution fluorescence microscopy of Lambda DNA. [Abadi et al. Entangled polymer dynamics beyond reptation, *Nature Communications* (2018).]





Polymer - fluid interaction

- Addition of high molecular weight polymers to a Newtonian fluid, even at low concentrations (ppm) imparts elasticity to the liquid, which can dramatically alter the macroscopic flow behaviour.
- E.g. drag reduction, enhanced pressure drop in porous media, inhibiting jet breakup, spray atomization.
- As polymers stretch in certain flow regions, they generate **localized elastic stresses** within the fluid. This is solved for in the model.



Holzner, M. (2018). Polymers reduce drag more than expected. *Physics*, 11, 29.



Polymer - particle interaction

 Polymer flocculants induce flocculation by neutralizing the surface charge of the particles or by forming bridges between individual particles.





Microstructure of kaolinite floc as revealed by cryo-SEM -Sharma, S., Lin, C. L., & Miller, J. D. (2017). Multi-scale features including water content of polymer induced kaolinite floc structures. Minerals Engineering, 101, 20-29.

- Adsorption mechanism needs to be modelled, no current techniques available in the literature and so this needs to be developed.
- **Bridging mechanism** will hence be implicit from adsorption.
- Adsorption is determined by attachment process, **hydrophobic** or **electrostatic interaction**.
- Hence attachment mechanism upon collision will rely on electrochemical properties of surface of particle and the polymer head / tail.



Polymer modelling: FENE chains

- FENE (finitely extensible nonlinear elastic) chain model represents the polymer as a sequence of beads connected by nonlinear springs.
- Springs used to model individual Kuhn chains





Polymer in equilibrium conditions



Polymer and system properties for equilibrium simulations

Property	Symbol	Value
Polymer species	-	λ -phage DNA
Contour length (μm)	l	21
Persistence length (μm)	λ_P	0.066
Effective persistence length (µm)	$\lambda_{P,eff}$	0.082
Bead radius (μm)	r_B	0.0693
Fluid dynamic viscosity (kgm ⁻¹ s ⁻¹)	μ_F	0.001
Fluid temperature (K)	Т	296
Simulation Euler timestep (<i>ms</i>)	Δt	0.01



Ensemble of polymers in equilibrium conditions





Ensemble of polymers under shear flow regime









Ensemble of polymers under shear flow regime - results



Shear flow simulation for Wi = 1.3, 6.3 and 76. Probability distribution functions of bead position within the domain (left) and mean polymer extension (right).



Polymer-fluid interaction

• Stress tensor in Navier-Stokes equations is altered to account for additional contribution from polymers.

$$\frac{\partial u_i}{\partial t} + u_j \frac{\partial u_i}{\partial x_j} = -\frac{1}{\rho_F} \frac{\partial P}{\partial x_i} + \frac{1}{\rho_F} (\tau_{ij}^s + \tau_{ij}^P)$$
$$\tau_{ij}^P = \frac{\mu_P}{\lambda_P} (f(r)c_{ij} - \delta_{ij})$$
$$f(r) = \frac{R_0^2 - 3}{R_0^2 - R^2}$$
$$c_{ij} = 3 < R_i R_j > \frac{1}{< R^2 > eq}$$

R: Spring extension

 R_0 : Maximum spring extension $< R^2 >$: Root-mean-square extension for full chain.

 μ_P : Polymeric solution viscosity



Polymer-laden turbulent flow



- Ratio of solvent to mixture viscosity, $\beta = 0.9$
- $Re_{\tau} = 180$



Polymer-laden turbulent flows



FIG. 3. Mean streamwise velocity normalized by shear velocity, u_{τ} , for turbulent channel flow at Re_{τ} =180.



FIG. 4. Root-mean-square of velocity fluctuations normalized by shear velocity, u_{τ} , for turbulent channel flow at Re_{τ} =180.



Polymer-laden turbulent flows







FIG. 6. Probability density distribution functions of mean polymer radius of gyration in turbulent channel flow simulation. Comparison of polymers located within individual flow regions.



Polymer-particle interaction



- Adsorption mechanism activates upon collision of bead with particle.
- Bead-spring force is two-way coupled with particle, with restoring force also exerted on particles.



Microstructure of kaolinite floc as revealed by cryo-SEM -Sharma, S., Lin, C. L., & Miller, J. D. (2017). Multi-scale features including water content of polymer induced kaolinite floc structures. Minerals Engineering, 101, 20-29.



Conclusions & further work

- FENE bead-spring polymer model has been developed and implemented in Nek5000, an open-source spectral-element based solver.
- After having validated the polymer dynamics in a simple quiescent case and a shear flow, a turbulent channel flow simulation was performed at $Re_{\tau} = 180$ which predicts mean and rms velocity fluctuations typical of a drag-reduced flow.
- We also observe how the various regions of the channel affect the deformation of the polymer chain such that polymers in the wall-region are more stretched and possess larger radii of gyration than their bulk flow counterparts.
- Polymer-particle interaction mechanism has been implemented and tested, with preliminary simulations exhibiting similar behaviour to that shown in experiments.
- This mechanism is now being used in a channel flow to determine the effects of polymer additives on flow mechanisms such as dispersion, deposition and agglomeration.



Other work on behavioural modification

Pending submission:

Mortimer, L. F. and Fairweather, M., TBC. Development of behavioural modification techniques through simulation of binary particle agglomeration events in isotropic turbulence.

Published:

Mortimer, L. F. and Fairweather, M., 2020. Density ratio effects on the topology of coherent turbulent structures in two-way coupled particle-laden channel flows. *Physics of Fluids*, *32*(10), p.103302. <u>doi: 10.1063/5.0017458</u>

Mortimer L. F., Njobuenwu D. O., Fairweather M. 2020. Agglomeration dynamics in liquid– solid particle-laden turbulent channel flows using an energy-based deterministic approach. *Physics of Fluids.* 32.4 doi: 10.1063/5.0001596

Mortimer L. F., Njobuenwu D. O., Fairweather M. 2019. Near-wall dynamics of inertial particles in dilute turbulent channel flows. *Physics of Fluids*. 063302-1-063302-19 31.6 doi:10.1063/1.5093391



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This work is supported by a UK Engineering and Physical Sciences Research Council grant at the University of Leeds from the TRANSCEND (Transformative Science and Engineering for Nuclear Decommissioning) project.



Engineering and Physical Sciences Research Council



Thank you for your attention!





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<u>Analysis of a Titanosilicate glass series – at least,</u> what the pandemic has permitted

Lucas-Jay Woodbridge, University of Sheffield

Transcend theme meeting, integrated waste management

Date: 02/12/20 Location: Mainly Oregon, Iowa and the Carolinas





<u>Analysis of a Titanosilicate glass series – at least, what</u> <u>the pandemic has permitted</u>



Ionsiv IE-911 received from NIS ltd (Tony Kay)

Lucas-Jay Woodbridge*



Powered respirator – image from arco.co.uk

2020 🗉 The University of Sheffield

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Re-visiting the glasses

- Why this chemistry
- Vitrification¹
- Glass success



2020 🛙 The University of Sheffield



The original material

- Framework Titanosilicate²
- Ionsiv-IE911³

Transformative Science and Engineering for Nuclear Decommissioning



C-axis view of Ionsiv IE-911⁴





03

3

T

Na

Ion exchange mechanism

- Ion exchange ^{3,5,6}
- Protonation step⁵
- Final uptake⁵



Protonated form of a framework titanosilicate⁵



C-axis view of Ionsiv IE-911 with Cs in tunnel structure⁴




2020 🛙 The University of Sheffield



Thermal analysis of glasses



 NS_2

NS

N₂S

Na₂O



Thermal analysis of glasses



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TRANSCEND

Plan going forward

- Melts
- Raman
- Verify Thermal data
- XAFS, XANES
- XRF
- Load lonsiv and repeat











Acknowledgements









HENRY ROYCE



midas

2020 🖸 The University of Sheffield

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Thank you

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Generation and Transport of Radiolytic Hydrogen in Hydroxide Sludges Mel O'Leary, DCF, The University of Manchester

NDA Transcend Conference

02/12/2019 NDA Transcend Conference





Introduction

Experimental Setup Transport Measurements Bubbles Conclusions







Introduction Experimental Setup

Transport Measurements Bubbles Conclusions



Experimental Setup













Highly collimated intense beam









TRANSCEND

Transformative Science and Engineering for Nuclear Decommissioning

Samples



Probes

12 samples in parallel







Probe



Dosimetry



Dosimetry



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Dosimetry





Introduction Experimental Setup Transport Measurements Bubbles Conclusions



Probe





Diffusion





1D Diffusion









Parameters from Fit



Transformative Science and Engineering for Nuclear Decommissioning Diffusion Coefficients



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TRANS

ENL





Introduction Experimental Setup Transport Measurements Bubbles Conclusions









Bubble Formation



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Introduction Experimental Setup Transport Measurements Bubbles Conclusions



Thank you


Optimising Magnesium-Silicate-Hydrate Cement Made From Brucite

Mercedes Baxter Chinery, Imperial College London





Background

- Sludges from Sellafield ponds need to be turned into a waste form
- Known to be rich in Mg(OH)₂
- A novel cement based on MgO and SiO₂ sets as strong as OPC
- Opportunity to use the waste as an encapsulating cement



Earlier Results

- Reproduced initial system
- Optimised by Zhang (DIAMOND, 2012)
- Compressive strength as expected
- Good dimensional stability









Current Work

- Investigating how replacing the MgO with Mg(OH)₂ affects
 - fluidity
 - setting
 - properties of the cement







Current Work

- Setting and measuring strength for properties
- Adapting water content and dispersants to improve fluidity
- ICP to investigate reactants available









Future Outlook

- Trials with artificial sludge from Sellafield
- Understand the durability properties of the cement



Thank you

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Radiation effects on nuclear waste forms: How does the degree of crystallinity in a glassceramic affect radiation tolerance?

Tamás Zagyva – The University of Manchester, Dalton Cumbrian Facility

Theme 1 Integrated Waste Management

2nd December 2020 Online



e University of Manchester Dalton Nuclear Institute







~ 300 less product canisters which offers ~ £55 million savings to the UK taxpayers [1].



1



PhD topic

Radiation effects on nuclear waste forms: How does the degree of crystallinity in a glass-ceramic affect radiation tolerance?





PhD topic

Radiation effects on nuclear waste forms: How does the degree of crystallinity in a glass-ceramic affect radiation tolerance?





Simple Ca/Zn GC samples Irradiation experiments

Crystalline phases in the VTR samples:

- powellite
- cerium zirconium oxide

VTR samples

zircon

- zinc chromite
- ruthenium oxide
- barium molybdate







VTR samples

Simple Ca/Zn GC samples

Irradiation experiments

VTR sample containing large powellite crystals

- horizontal cracks
- formed probably at a late stage (during cooling)









VTR samples

Simple Ca/Zn GC samples

Irradiation experiments

VTR sample containing <u>large zircon crystals</u>

- cracks mostly around the crystals
- formed probably at a late stage (during cooling)











HT 15.0 kV Magnification 1000 x – 100 µm –

850 °C

36









Thank you for the help!

Laura Leay Brian O'Driscoll

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